

Divide eqn (9) by (10)

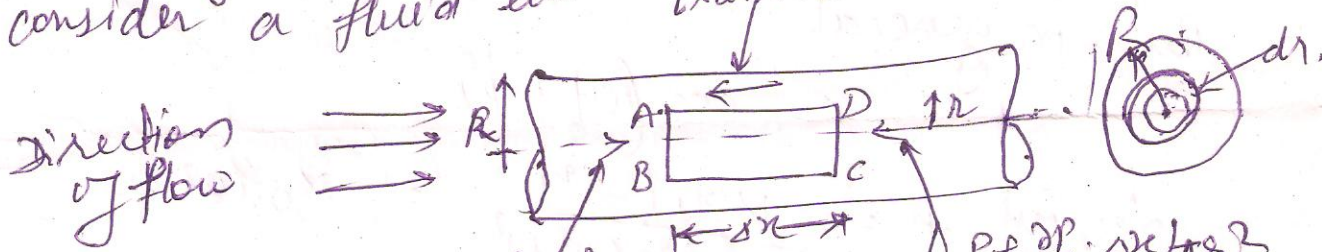
$$\frac{x_0 \sin \phi}{x_0 \cos \phi} = \frac{-2\mu r \frac{dv}{dr}}{(1-r^2)^2 - (2\mu r)^2} \times \frac{(1-r^2) - (2\mu r)^2}{\mu r (1-r^2)}$$

$$\tan \phi = -\frac{2\mu r}{(1-r^2)}$$

Unit-5 / viscous Flow / F.M

* Relation between shear stress, pressure gradient and velocity distribution :-

consider a horizontal pipe of radius R . The viscous fluid is flowing from left to right as shown in fig. consider a fluid element



of radius r is ~~flow~~ sliding in cylindrical fluid element of radius $(r+dr)$. let P is the pressure at face AB & $(P + \frac{dP}{dx} \cdot \Delta x)$ is pressure at CD. the pressure forces acting on fluid element ABCD.

- ① Pressure force on AB = $P \pi r^2$
 - ② " " " " face CD = $(P + \frac{dP}{dx} \cdot \Delta x) \pi r^2$
 - ③ shear force $\tau \times 2\pi r \Delta x$ on surface on the
- As there is no acceleration therefore the summation of pressure forces will be zero.

$$\therefore P \pi r^2 - (P + \frac{dP}{dx} \cdot \Delta x) \pi r^2 - (\tau \times 2\pi r \Delta x) = 0$$

$$- \frac{dP}{dx} \cdot \Delta x \pi r^2 - \tau \times 2\pi r \Delta x = 0$$

$$- \frac{dP}{dx} \cdot r - \tau = 0$$

$$\tau = - \frac{dP}{dx} \cdot \frac{r}{2}$$

New velocity distribution

we know $\tau = \mu \frac{du}{dy}$, but here y is measured from pipe wall

$$\therefore y = R - r \text{ or } dy = -dr$$

$$\tau = -\mu \frac{du}{dr} \quad \text{substituting } \textcircled{1}$$

$$-\frac{\partial p}{\partial x} \cdot \frac{r}{2} = -\mu \frac{du}{dr}$$

$$= \frac{\partial p}{\partial x} \frac{r}{2} = \mu \frac{du}{dr} \text{ or } \mu \frac{du}{dr} = \frac{\partial p}{\partial x} \frac{r}{2}$$

As $\frac{\partial p}{\partial x}$ is const. Integrating w.r.t r

$$\mu \int du = \int \frac{1}{2} \mu \left(\frac{\partial p}{\partial x} \right) \cdot r \cdot dr$$

$$\Rightarrow u = \frac{1}{2\mu} \frac{\partial p}{\partial x} \cdot \frac{r^2}{2} + C$$

$$\therefore u = \frac{1}{4\mu} \frac{\partial p}{\partial x} r^2 + C$$

for finding C , put $r = R$ & $u = 0$

$$0 = \frac{1}{4\mu} \frac{\partial p}{\partial x} R^2 + C$$

$$\therefore u = \frac{1}{4\mu} \frac{\partial p}{\partial x} r^2 - \frac{1}{4\mu} \frac{\partial p}{\partial x} R^2$$

$$= -\frac{1}{4\mu} \frac{\partial p}{\partial x} [R^2 - r^2]$$

Ratio of max. to average velocity:-

$$u_{\max} = -\frac{1}{4\mu} \frac{\partial p}{\partial x} R^2$$

Average velocity = $\frac{Q}{A_{\text{area}}}$

$dQ =$ velocity at radius $r \times$ element ring area

$$= u \times 2\pi r dr$$

$$= -\frac{1}{4\mu} \frac{\partial p}{\partial x} (R^2 - r^2) 2\pi r dr$$

$$= -\frac{\pi}{2\mu} \frac{\partial p}{\partial x} (R^2 r - r^3) dr$$

$$Q = \int_0^R \frac{\pi}{2\mu} \left(\frac{\partial p}{\partial x} \right) \left(\frac{R^2 r}{2} - \frac{r^3}{4} \right) dr$$

$$= Q = \frac{\pi}{2\mu} \left(-\frac{\partial p}{\partial n} \right) \left[\frac{R^7}{2} - \frac{R^4}{4} \right]$$

$$Q = \frac{\pi}{8\mu} \left(\frac{\partial p}{\partial n} \right) R^4$$

$$\bar{u} = \frac{\frac{\pi}{8\mu} \left(-\frac{\partial p}{\partial n} \right) R^4}{\pi R^2} = \frac{1}{8\mu} \left(-\frac{\partial p}{\partial n} \right) R^2$$

$$\therefore \frac{u_{max}}{\bar{u}} = \frac{-\frac{1}{4\mu} \left(\frac{\partial p}{\partial n} \right) R^2}{-\frac{1}{8\mu} \frac{\partial p}{\partial n} R^2} = \underline{\underline{2.0}}$$

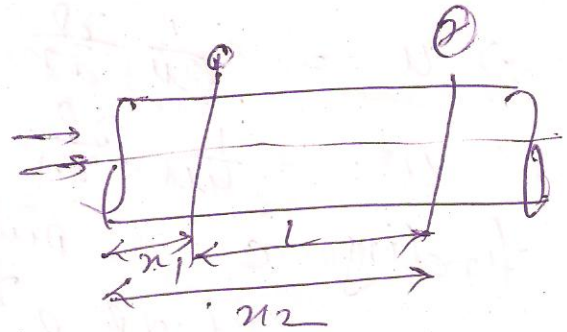
* Drop of pressure for a given length (L) of a pipe :-

we know

$$\bar{u} = \frac{1}{8\mu} \left(-\frac{\partial p}{\partial n} \right) R^2$$

$$-\frac{\partial p}{\partial n} = \frac{8\mu \bar{u}}{R^2}$$

Integrate with n -



$$= (p_1 - p_2) = \frac{8\mu \bar{u}}{R^2} \cdot [n_1 - n_2]$$

$$= (p_1 - p_2) = \frac{8\mu \bar{u} (n_2 - n_1)}{R^2}$$

$$[\because n_2 - n_1 = L]$$

$$(p_1 - p_2) = \frac{8\mu \bar{u} \cdot L}{R^2} = \frac{8\mu \bar{u} L}{(D/2)^2}$$

$$= \frac{32 \mu \bar{u} \cdot L}{D^2}$$

But $\frac{p_1 - p_2}{\rho g}$ is pressure head $\frac{p_1 - p_2}{\rho g} = H_f$

$$\therefore \frac{p_1 - p_2}{\rho g} = \frac{32 \mu \bar{u} \cdot L}{\rho g D^2}$$

The above is called Hagen Poiseuille formula